

# Improved Fluid-Model of TCP/AQM Network for Congestion Control

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**Abstract:** In this paper, recently proposed active queue management (AQM) algorithms for supporting end-to-end transmission control protocol (TCP) congestion control is revisited. We focus recently developed theoretic results on design and analysis for the AQM based TCP congestion control dynamics. In this context, the existing fluid model of the TCP/AQM network is discussed. Moreover, an improved fluid model is addressed, taking time delay in inner feedback loop into account, which is neglected in the modeling process of fluid model. The stabilization of the fluid model is investigated, which has shown that the stabilizing region of PID congestion controller for the conventional fluid model moves  $\frac{1}{k}$  and  $\frac{T_1}{k}$  along the  $k_p$  and  $k_d$  axes respectively compared with that for the improved fluid model, ie. the actual stability region. The improved fluid model has a great potential in analyzing and designing various network congestion control algorithms.

## 1. INTRODUCTION

State-of-the-art Internet is a decentralized control system employing dynamic Transmission Control Protocols at the sources and Active Queue Management protocols at the routers. The predominant transmission control protocol suites are variants of TCP [1]. TCP flow control is the most important mechanism for congestion control in IP networks. Since Jacobson proposed the end-to-end flow control scheme in 1988 [1], there have been many enhanced and improved versions, such as Tahoe, Reno, New Reno, SACK and Vegas [2-4]. However, these works merely pay attention to the end system. Recent attention has been drawn to explore how to use the intermediate node to avoid congestion because there is a limit to how much control can be accomplished at the end system. AQM [5-7], as one class of packet dropping/marketing mechanism in the router queue, has been recently proposed to support end-to-end congestion control in the Internet. It has been a very active research area in the Internet community. The goals of AQM are as follows: (a) to reduce the average length of queues in routers and thereby decrease end-to-end delay experienced by packets; (b) to ensure that network resources are used efficiently by reducing packet loss that occurs when queues overflow. A fluid-flow model of TCP behavior is developed in [8], up to now, which is extensively employed to design various AQM

algorithm from the viewpoint of control theory and control engineering [9, 10]. However, time delay in inner feedback loop is neglected in the modeling process of fluid model, which will result that the stability region derived from the conventional fluid model is not an accurate representation of the actual stability region.

The paper is organized as follows: Sections 2 is devoted to introduce fluid-based network model of TCP/AQM network. An Improved fluid-model of TCP/AQM network is proposed and described in Section 3, including the theoretical analysis and simulation experiments. Finally, Section 4 concludes the paper.

## 2. FLUID-BASED NETWORK MODEL OF TCP/AQM NETWORK

In [8], a dynamic model of TCP behavior was developed using fluid-flow and stochastic differential equation analysis. Simulation results demonstrated that the model accurately captured the dynamics of TCP. In this paper we use a simplified version of that model which ignores the TCP timeout mechanism. This model relates the average value of key network variables and is described by the following coupled, nonlinear differential equations:

$$\begin{aligned}\dot{W}(t) &= \frac{1}{R(t)} - \frac{W(t)W(t-R(t))}{2R(t-R(t))} p(t-R(t)) \\ \dot{q}(t) &= \frac{W(t)}{R(t)} N(t) - C\end{aligned}\quad (1)$$

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$$\begin{aligned}
 G_p(s) &= \frac{Q(s)}{P(s)} = \frac{W(s)}{P(s)} \cdot \frac{Q(s)}{W(s)} \\
 &= G_{TCP}(s)G_{queue}(s) \\
 &= \frac{ke^{-R_0s}}{(T_1s+1)(T_2s+1+e^{-R_0s})} \tag{6}
 \end{aligned}$$

Where  $k = \frac{(R_0C)^3}{4N^2}$ ,  $T_1 = R_0$ ,  $T_2 = \frac{R_0^2C}{2N}$ .

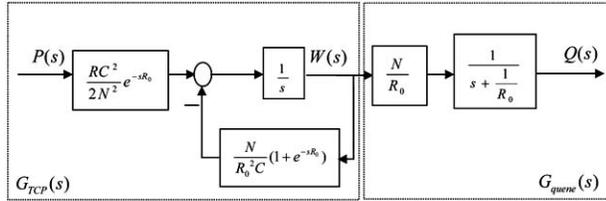


Fig. (3). Block-diagram of the improved fluid model.

### 3.2. Stability Analysis of the Improved Fluid-Model

**Lemma 3.1:** The plant  $G_p(s)$  defined in (6) is stable for

all positive values of  $R_0 \square C$  and  $N$ .

**Proof:**

Since

$$\begin{aligned}
 G_p(s) &= \frac{ke^{-R_0s}}{(T_1s+1)(T_2s+1+e^{-R_0s})} \\
 &= \frac{ke^{-R_0s}}{(T_1s+1)(T_2s+1)(1+\frac{e^{-R_0s}}{T_2s+1})} \\
 &= \frac{ke^{-R_0s}}{(T_1s+1)(T_2s+1)} \cdot \frac{1}{1+\frac{e^{-R_0s}}{T_2s+1}}
 \end{aligned}$$

Apparently, for all positive values of  $R_0$ ,  $C$  and  $N$ ,

$T_1 = R_0$  and  $T_2 = \frac{R_0^2C}{2N}$  are positives, so the zeros of the

transfer function  $(T_1s+1)$  and  $(T_2s+1)$  are in the left-half part of the complex plane for all values of the parameters

$R_0 \square C$  and  $N$ .

For  $(1 + \frac{e^{-R_0s}}{T_2s+1})$ , we have

$$\left| \frac{e^{-R_0s}}{T_2s+1} \right|_{s=j\omega} = \frac{1}{\sqrt{(T_2\omega)^2 + 1}} < 1$$

According to the Nyquist stability test zero of the transfer function  $(1 + \frac{e^{-R_0s}}{T_2s+1})$  is also in the left-half part of the complex plane for all values of the parameters  $R_0$ ,  $C$  and  $N$ .

So we can thus conclude that the plant  $G_p(s)$  defined in (6)

is always stable for all positive values of  $R_0$ ,  $C$  and  $N$ .

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### 3.3. Control Analysis of the Improved Fluid-Model

The closed-loop Block-diagram of TCP/AQM congestion control system is shown in Fig. (4), then the closed-loop transfer-function of the system becomes

$$\phi(s) = \frac{C(s)G_p(s)}{1 + C(s)G_p(s)} \tag{7}$$

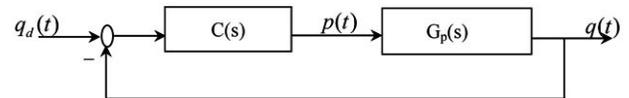


Fig. (4). Block-diagram of the TCP/AQM congestion control system.

**Lemma 3.2:** For PID controller of TCP/AQM network, the whole size and shape of the stabilizing region of  $(k_p, k_i, k_d)$  designed based on fluid model is equal to that

designed by the improved fluid model, however it moves  $\frac{1}{k}$

and  $\frac{T_1}{k}$  along the  $k_p$  and  $k_d$  axes respectively compared with

that designed based on the improved fluid model. Since the later more accurately models the dynamics of the TCP/AQM network than the former, which imply that there exists error in the stabilizing region of the PID-type congestion controller designed based on fluid model.

**Proof:**

The transfer function of PID controller is :

$$C(s) = k_p + \frac{k_i}{s} + k_d s = \frac{k_i + k_p s + k_d s^2}{s} \quad (8)$$

where  $k_p$ ,  $k_i$  and  $k_d$  are coefficient of proportional, differential and integral respectively.

Upon substitution by (4), the closed-loop characteristic equation of the system shown in Fig. (2) becomes

$$\Delta'(s) = (T_1 s + 1)(T_2 s + 1)s + k(k_i + k_p s + k_d s^2)e^{-R_0 s} \quad (9)$$

And substitution by (6), the closed-loop characteristic equation of the system shown in Fig. (3) as

$$\Delta(s) = (T_1 s + 1)(T_2 s + 1 + e^{-R_0 s})s + k(k_i + k_p s + k_d s^2)e^{-R_0 s} \quad (10)$$

Eqn.10 can be rewritten in the form

$$\begin{aligned} \Delta(s) &= (T_1 s + 1)(T_2 s + 1)s \\ &+ k\left[\left(k_i + \left(k_p + \frac{1}{k}\right)s + \left(k_d + \frac{T_1}{k}\right)s^2\right)\right]e^{-R_0 s} \\ &= (T_1 s + 1)(T_2 s + 1)s + k(k'_i + k'_p s + k'_d s^2)e^{-R_0 s} \end{aligned} \quad (11)$$

Apparently eqn. 11 is the same as eqn.9 in form, where  $k'_p = k_p + \frac{1}{k}$ ,  $k'_i = k_i$  and  $k'_d = k_d + \frac{T_1}{k}$ , is the designed controller's parameter designed based on the fluid model, ie.eqn. 4.  $k_p$ ,  $k_i$  and  $k_d$  is the designed controller's parameter designed based on the improved fluid model.

For

$$k'_p = k_p + \frac{1}{k}, \quad k'_i = k_i, \quad k'_d = k_d + \frac{T_1}{k} \quad (12)$$

Thus we can conclude that the whole size and shape of the stabilizing region of  $(k_p, k_i, k_d)$  is not changed, but it

move  $\frac{1}{k}$  and  $\frac{T_1}{k}$  along the  $k_p$  and  $k_d$  axes respectively compared with that designed according to the improved fluid model.

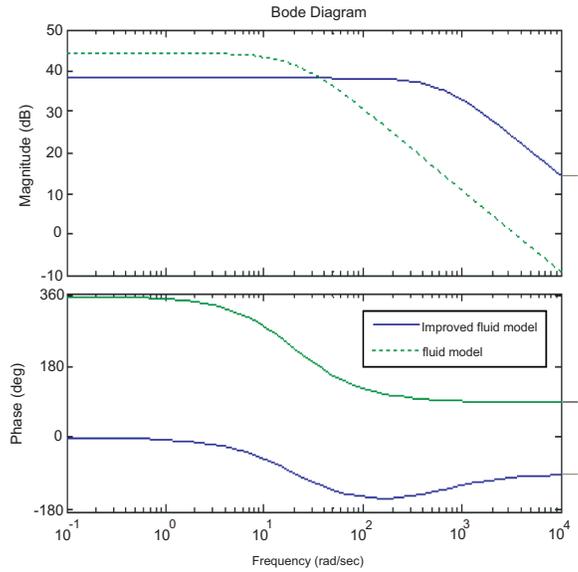
**Remark 1** For proportional and proportional-integral congestion controller the whole size and shape of the stabilizing region of  $k_p$  and  $(k_p, k_i)$  is not changed, but it move  $\frac{1}{k}$  along the  $k_p$  axes compared with that designed according to the improved fluid model.

**Remark 2** since  $\frac{1}{k} = \frac{4N^2}{(R_0 C)^3}$  and  $\frac{T_1}{k} = \frac{4N^2}{C(R_0 C)^2}$ , so the error of the stabilizing region of congestion controller will become more bigger, with big  $N$ , and small  $R_0$  or  $C$ .

**4. SIMULATION ANALYSIS**

**Case 1:** The parameter of the TCP/AQM network is equal to that in paper [12] and the expected queue length size is 150 packets so the improved fluid model is

$$G_p(s) = \frac{164.8e^{-0.05s}}{(0.05s + 1)(0.046875s + 1 + e^{-0.05s})}$$



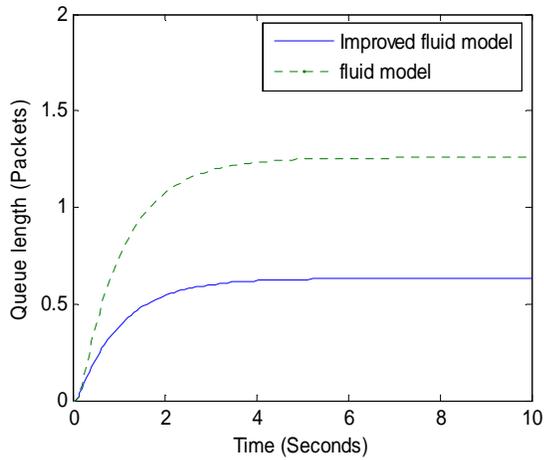
**Fig. (5-a).** Bode plot of network model in paper [12].

Figs. (5-a) are magnitude plots and phase plots, the solid lines indicate the improved fluid model, while the dash lines show the fluid model. We can see that these two models can not match very well.

The RED congestion controller design in [12] is

$$C(s) = \frac{5.125 \times 10^{-5}}{0.97745s + 1}$$

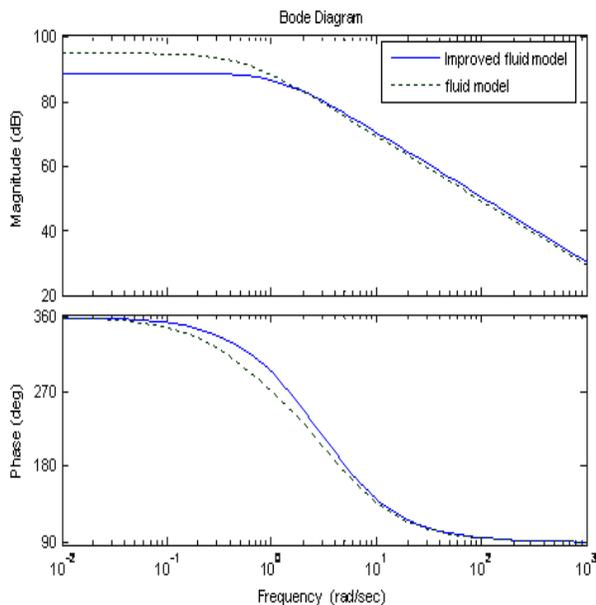
and the simulation result is shown as Fig. (5-b).



**Fig. (5-b).** The simulation result of RED congestion controller design in paper [12].

**Case 2:** the parameter of the TCP/AQM is equal to that in [8], and the expected queue length size 150 is packets, so the improved fluid model is

$$G_p(s) = \frac{54517.6e^{-0.246s}}{(0.246s + 1)(1.891s + 1 + e^{-0.246s})}$$

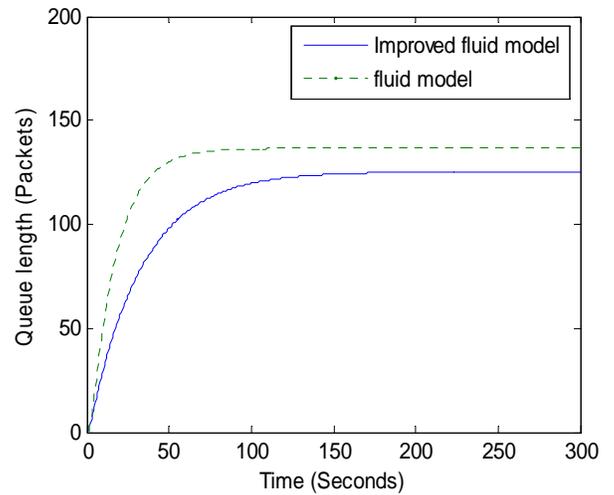


**Fig. (6-a).** Bode plot of network model in paper [11].

Figs. (6-a) are magnitude plots and phase plots, the solid lines indicate the improved fluid model, while the dash lines show the fluid model. We can see that these two models can wholly match each other.

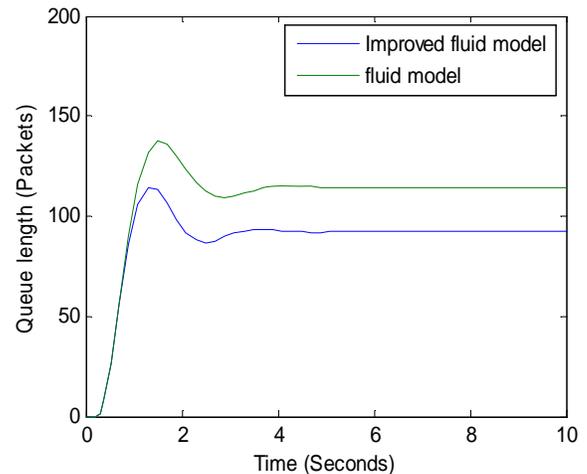
(1) RED congestion controller:

$$C(s) = \frac{9.3 \times 10^{-7}}{s + 0.005}$$



**Fig. (6-b).** The simulation result of RED congestion controller design in paper [11].

and the simulation result is shown in Fig. (6-b).



**Fig. (6-c).** The simulation result of the proportional congestion controller design in paper [11].

(2) Proportional congestion controller:

$$C(s) = 5.8624 \times 10^{-5},$$

and the simulation result is shown in Fig. (6-c).

(3) Proportional plus integration congestion controller:

$$C(s) = 9.64 \times 10^{-6} \left( 1.8868 + \frac{1}{s} \right),$$

and the simulation result is shown in Fig. (6-d).

**Case 3:** the parameter of the TCP/AQM is equal to that in [13] and the expected queue length size is 150 packets so the improved fluid model is

$$G_p(s) = \frac{234375e^{-0.4s}}{(0.4s + 1)(5s + 1 + e^{-0.4s})}$$

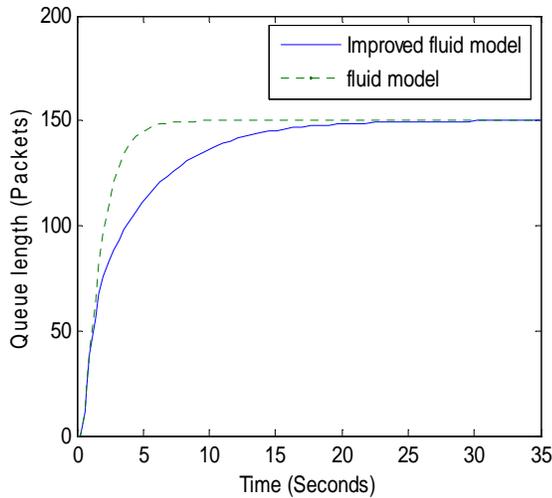


Fig. (6-d). The simulation result of PI controller design in paper [11].

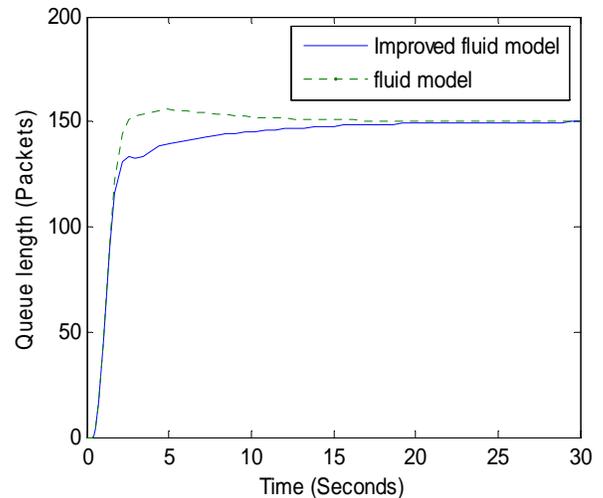


Fig. (7-b). The simulation result of the PID controller design in paper [13].

Figs. (7-a) are magnitude plots and phase plots, the solid lines indicate the improved fluid model, while the dash lines show the fluid model. We can see that these two models can wholly match each other.

Figs. (8-a) are magnitude plots and phase plots, the solid lines indicate the improved fluid model, while the dash lines show the fluid model. We can see that these two models can not match each other.

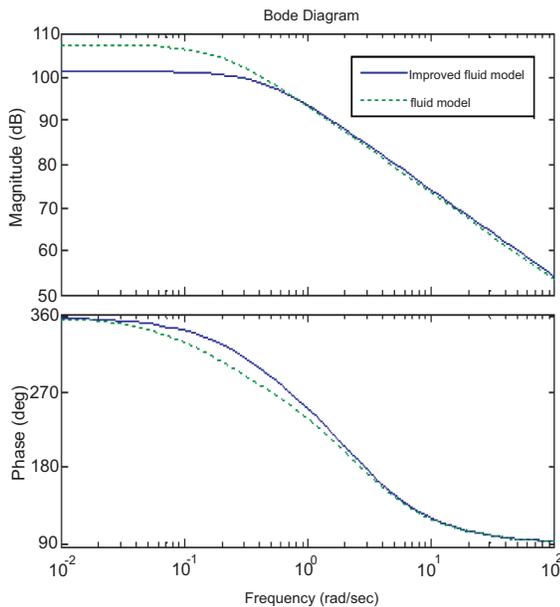


Fig. (7-a). Bode plot of the network model in paper [13].

The controller’s parameters is equal to that in paper [13], and the simulation result is shown in Figs. (7-b).

Case 4: The parameter of the TCP/AQM is as  $C=1200$ packets/s,  $R=0.01$ s,  $N=30$ , and the expected queue length size is 150 packets so the improved fluid model is

$$G_p(s) = \frac{0.48e^{-0.01s}}{(0.01s + 1)(0.002s + 1 + e^{-0.01s})}$$

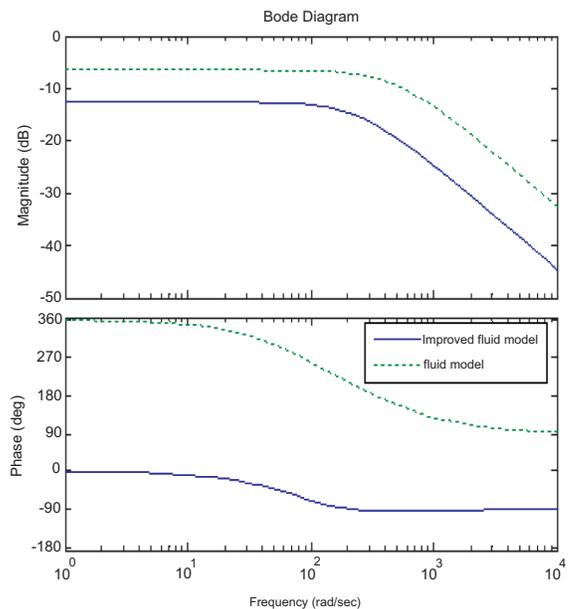
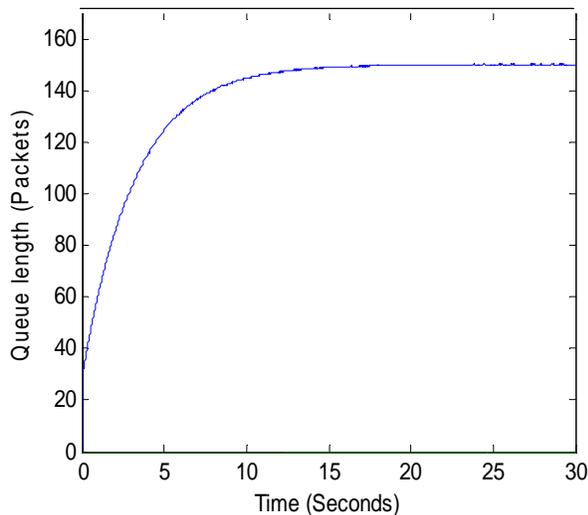


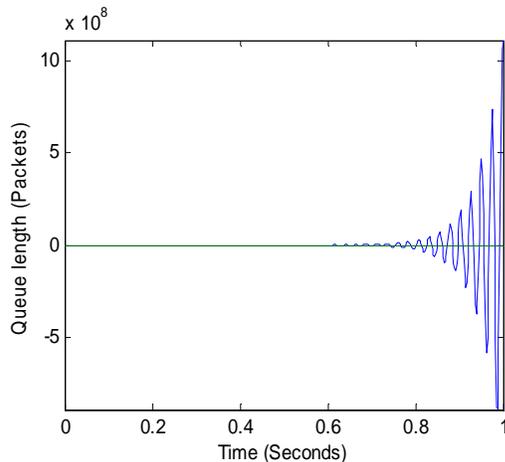
Fig. (8-a). Bode plot of the network model.

The PID controller parameters is  $k_p = 0.5$ ,  $k_i = 0.8$ ,  $k_d = 0.01$ , and the simulation result is shown in Figs. (8-b) and Figs. (8-c).

From the above bode plot based analysis, we can find that the dynamics of the fluid model is different from that of the improved fluid model. Since the later more accurately models the dynamics of the TCP/AQM network than the former, which imply that there exists modeling error in the



**Fig. (8-b).** The simulation result of the PID controller by fluid model.



**Fig. (8-c).** The simulation result of the PID controller by improved fluid model.

former. Furthermore, the simulation results have shown that one congestion controller designed based on fluid model maybe can not obtain satisfactory performance just as Fig. (5-b), Fig. (6-b), Fig. (6-c), Fig. (6-d), Fig. (7-b) and Fig. (8) demonstrated.

## 5. CONCLUSION AND DISCUSSION

In this study, we firstly point out the invalidity of popular fluid model of TCP/AQM network through theoretical analysis and simulation experiments. By considering the time delay in the inner feedback loop, which is neglected in the modeling process of fluid model, we present an improved fluid model. The theoretical analysis has shown that the whole size and shape of the stabilizing region of PID con-

gestion controller designed based on fluid model is not changed, but it move  $\frac{1}{k}$  and  $\frac{T_1}{k}$  along  $k_p$  and  $k_d$  axes respectively compared with that designed based on the improved fluid model which more accurately represent the dynamic of the TCP/AQM network. This improved fluid model has a great potential in analyzing and designing various network congestion control algorithms.

## NOMENCLATURE

TCP	=	Transmission Control Protocols
AQM	=	Active Queue Management

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